# **NOx emission control for Coke Oven**

Application of Two-Staged combustion to the single-staged combustion chamber

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posco

# **1. POSCO at a Glance**

POSCO, the history of Korean steel industry built from literally NOTHING
Steel, fundamental material of national economy supporting other industries





#### • Air quality standards

			dards		lonon		
		2001~	2007~	USA	Japan	WHO	
NO <sub>2</sub> (ppm)	1hour	0.15	0.10	-	-	0.105	
	24hour	0.08	0.06	-	0.04~ 0.06	-	
	Year	0.05	0.03	0.053	-	0.021	

#### Chimney emission standards

	O <sub>2</sub> %	2010~2014	2015~
Sinter plant	15	<b>220</b> <sup>1)</sup> / <b>120</b> <sup>2)</sup>	<b>200</b> <sup>1)</sup> / <b>120</b> <sup>2)</sup>
Reheating furnace	11	<b>200</b> <sup>1)</sup> / <b>150</b> <sup>2)</sup>	<b>200</b> <sup>1)</sup> / <b>150</b> <sup>2)</sup>
Coke Oven	7	250	250/150 <sup>3)</sup>
Power Generator	15	100 <sup>4)</sup> / 50 <sup>5)</sup>	80/50/20 <sup>6)</sup>

<sup>1)</sup> Built before 2007. Jan <sup>2)</sup> Built after 2007.Feb <sup>3)</sup> Built after 2007.Jan <sup>4)</sup> Built before 2001. Jun <sup>5)</sup> Built after 2001.Jul , <sup>6)</sup> built after 2017. Jan

Following the adoption of PM 2.5 standard which will be effective in 2015,

the government is going to regulate PM2.5 emissions from stacks

 $\rightarrow$  NOx control is essential to reduce PM2.5

# **3. Coke Ovens at Pohang Works**

### Pohang works operates single stage combustion chamber Coke Oven





구분	#1 Coke plant			#2 Coke plat				#3 Coke plant		
Battery	1	2	3	4	5	6	7	8	9	10
Built year	1973	1976		1978		1981		1983	2009	
Combustion	stion Single staged combustion						Two staged			

# 4. Coke oven & NOx emission

### Schematic diagram of Coke Oven combustion chamber



Steel Solution for Green Growth

# **5. NOx emission control techniques**

#### **5.3.12.2 Reduction of NO<sub>x</sub> by primary measures**

" waste gas recirculation: The lower  $O_2$  and higher  $CO_2$  concentrations reduce the flame temperature.

" staged air combustion: by adding the combustion air in several stages, combustion conditions become more moderate, and  $NO_X$  formation is reduced

 Iowering coking temperatures: A lower coking temperature requires a lower heating chamber temperature, which results in less NO<sub>x</sub> formation.

For existing modern plants which have already incorporated low-NO<sub>x</sub> techniques, such as staged air combustion and waste gas recirculation, NO<sub>x</sub> concentrations of  $322 - 414 \text{ mg/Nm}^3(150 \sim 200 \text{ ppm})$  at 5 % O<sub>2</sub> are reported.

For existing plants without process-integrated deNO<sub>x</sub> measures, achievable levels for NOX are in the higher range up to 1783 g/t coke, with concentrations up to 1700 mg/Nm<sup>3</sup>(830ppm) at 5 % O<sub>2</sub>.

### 5.3.12.3 Reduction of $NO_x$ by secondary measures Description

 NOX emissions from coke oven firing are preferably minimized by process-integrated measures, but end-of-pipe techniques may also be applied. (applicable only to new plant)

*Reference : EU Best Available Techniques (BAT) Reference Document for Iron and Steel Production* 2012 March

- **5. NOx emission control techniques** 
  - How to reduce NOx for the conventional Coke Oven
    - **C** Application of SCR ?
      - Only applicable to New Plant
    - Lowering Coking temperature ?
      - Decrease the Coke productivity
    - Installation of Staged air combustion ?
      - Need to restructure of Coke Oven (refractory)



### **5. NOx emission control techniques**

 Concept diagram of two staged combustion using conventional Coke Oven



#### TRIZ tool was introduced to find out the solution

- Technical contradiction (temperature  $\downarrow \Rightarrow$  quality  $\downarrow$  , temperature  $\uparrow \Rightarrow$  quality  $\uparrow$ )
- Forty principles : Segmentation, Asymmetry õ

## 6. Pilot test at the #1 Coke Oven (19 combustion chambers)

#### Conditions for stable operation

#### ① Determination of secondary combustion air flow rate

- Total air flow rate : 12,800Nm3/hr (3% O2, mixed gas calorific value 1000 Kcal/Nm3 )
- Secondary air flow rate : 30% of total flow rate (benchmarked at the #10 Coke Oven) = 3,840Nm<sup>3</sup>/hr



#### **② Measuring Scarping Blower flow rate**



- [Scarping Blower Air flow rates]
- S/B : 5100Nm<sup>3</sup>/hr (Static pressure 260mmH<sub>2</sub>O)
- Not appropriate since it had low static pressure (requires > 1,000 mmH<sub>2</sub>O)

#### 6. Pilot test at the #1 Coke Oven

#### **③ Maintaining optimal Coke Oven Pressure**

- Target : O2 contents 2-4%, Pressure : 1.5 . 3.5 mmH2O)
- Waste gas pressure was measured to adjust top pressure by adjusting damper







#### **④** NOx Emission measurement

- CMS was installed on the chimney



# 7. Results of the test

### Operation conditions were identified

- Secondary air flow rate : 4,100Nm<sup>3/</sup>hr (32% of total air flow rate)
- Coke rate : 115%, Temperature : 1088  $^\circ\!\!{\rm C}$
- $O_2$  contents : 2-4%, Top pressure : 1.5 . 3.5 mmH<sub>2</sub>O

## Dramatic reduction of NOx

- 45% reduction (220ppm  $\rightarrow$  120ppm)



# 8. Replication at the #8 Coke Oven (76 combustion chambers)

#### Replicated at the larger scale Coke Oven

- Period : 2010. Sep ~ 2011.Jan / Expenditure : 1.7 billion Won
- New air blower for supplying secondary combustion air



#### Cost analysis

Index		POSCO Technology	SCR
Investment cost	Billion Won	1.7	6.2
<b>Operation cost</b>	(approx. 0.9 M\$)	0.4	1.5

Much more economical than end-of-pipe technology

# 9. Conclusions

- POSCO successfully reduced 45% of NOx emission at the conventional Coke Oven by applying secondary combustion air through COG scarping pipe.
- NOx emission control technology was successfully replicated at the #8 coke oven plant and it is under installation in other Ovens at the Pohang works.
- POSCO continues its efforts on developing new environmental technology